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(54) Title: POLYMER COMPOSITIONS**(57) Abstract**

Novel polyethylenes are prepared having a density in the range 900–980 kg/m³ and a molecular weight >200,000 characterised by a fracture toughness at –40 °C >20kJ/m² and a dynamic viscosity of <3000 Pa.s at 100 rad/sec. The novel polymers also having a die swell of 10–80 % and show a unique combination of physical and processing properties. The polymers may be prepared by use of catalysts comprising a metallocene component and a Ziegler component.

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POLYMER COMPOSITIONS

The present invention relates to novel polymer compositions and in particular to polymer compositions having improved physical properties as well as improved processability.

In recent years there have been many advances in the production of

5 polyolefin copolymers due to the introduction of metallocene catalysts. Metallocene catalysts offer the advantage of generally higher activity than traditional Ziegler catalysts and are usually described as catalysts which are single-site in nature. Because of their single-site nature the polyolefin copolymers produced by metallocene catalysts often are quite uniform in their molecular

10 structure. For example, in comparison to traditional Ziegler produced materials, they have relatively narrow molecular weight distributions (MWD) and narrow Short Chain Branching Distribution (SCBD). By narrow SCBD, it is meant that the frequency of short chain branches, formed where comonomers incorporate into the polyolefin chain, is relatively independent of molecular weight. Although

15 certain properties of metallocene products are enhanced by narrow MWD, difficulties are often encountered in the processing of these materials into useful articles and films relative to Ziegler produced materials. In addition, the uniform nature of the SCBD of metallocene produced materials does not readily permit certain structures to be obtained.

20 One approach to improving processability has been the inclusion of long chain branching (LCB), which is particularly desirable from the viewpoint of improving processability without damaging advantageous properties. US Patent No.s 5,272,236; 5,278,272; 5,380,810; and EP 659,773, EP 676,421, relate to the production of polyolefins with long chain branching.

25 Another approach is the addition of the polymer processing aids to the

polymer prior to fabrication into films or articles. This requires extra processing and is expensive.

A different approach to the problem has been to make compositions which are blends or mixtures of individual polymeric materials with the aim being to

5 maximise the beneficial properties of given components while minimising its processing problems. This also requires extra processing which increases the cost of materials produced. US Patent No.s 4,598,128; 4,547,551; 5,408,004; 5,382,630; 5,583,631; and 5,326,602; and WO 94/22948 and WO 95/25141 relate to typical blends.

10 Another way to provide a solution to the processability problems and to vary SCBD has been the development of various cascade processes, where the material is produced by a series of polymerisations under different reactor conditions, such as in a series of reactors. Essentially, a material similar in some ways to a blend is produced, with a modality greater than one for various physical

15 properties, such as the molecular weight distribution. While polyolefin compositions with superior processability characteristics can be produced this way, these methods are expensive and complicated relative to the use of a single reactor. Processes of interest are disclosed in US Patent No. 5,442,018, WO 95/26990, WO 95/07942 and WO 95/10548.

20 Another potentially feasible approach to improving processability and varying SCBD has been to use a multicomponent catalyst. In some cases, a catalyst which has a metallocene catalyst component and a conventional Ziegler-Natta catalyst component are used on the same support to produce a multimodal material. In other cases two metallocene catalysts have been used in polyolefin

25 polymerisations. Components of different molecular weights and compositions are produced in a single reactor operating under a single set of polymerisation conditions. This approach however is difficult from the point of view of process control and catalyst preparation. Catalyst systems of interest are disclosed in WO 95/11264. The polymer produced in this disclosure are blends of polymers having

30 a bimodal molecular weight distribution. They are also prepared specifically in a gas phase fluidised bed reactor.

We have now surprisingly found novel polyethylene compositions which exhibit both improved physical properties exemplified by their initial fracture toughness and improved processability as exemplified by their dynamic viscosity.

35 The novel polyethylenes also show a high density and high molecular weight.

Thus according to the present invention there is provided a polyethylene having an annealed density in the range 900 to 980 kg/m³ and a molecular weight greater than 200,000 characterised in that the polyethylene has

- (a) an initiation fracture toughness (G_p) at -40°C of greater than 20 kJ/m²,
- 5 (b) a dynamic viscosity of < 3000 Pa.s at 100 rad/sec (190°C) and < 3000 kPa.s at 0.01 rad/sec (190°C); and
- (c) a mass flow rate (MFR) under 21.6 kg load (190°C) of
0.01 - 100g/10 min.

Preferably the polyethylene according to the present invention has a
10 fracture toughness greater than 25kJ/m², a dynamic viscosity < 2500 Pa.s at 100 rad/sec (190°C) and < 1500 kPa.s at 0.01 rad/sec (190°C) and a MFR of 0.2-10g/10 min (21.6 kg load).

The preferred density for the polyethylenes of the present invention is in the range 930 to 970 kg/m³ and a molecular weight preferably greater than 400,000.

15 The polyethylenes of the present invention may also be characterised by having a die swell in the range 10-80%.

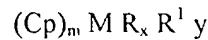
Thus according to another aspect of the present invention there is provided a polyethylene having an annealed density in the range 900-980 Kg/m³ and a molecular weight greater than 200,000 characterised in that the polyethylene has
20 (a) an initiation fracture toughness (G_p) at -40°C of greater than 20 kJ/m²
(b) a dynamic viscosity of <3000 Pa.s at 100 rad/sec (190°C) and
<3000 Kpa.s at 0.01 rad/sec (190°C), and
(c) a die swell in the range 10 - 80%.

25 The polyethylenes of the present invention preferably have a die swell in the range 20-40%.

The novel polyethylenes of the present invention may suitably be prepared by use of a multisite catalyst having two catalytic components. For example a Ziegler component and a component based on a metallocene complex.

Alternatively the multisite catalyst may comprise two metallocene components.

30 Examples of suitable metallocene components are complexes which may be represented by the general formula:



wherein Cp is a substituted or unsubstituted cyclopentadienyl nucleus; M is a Group IVA, VA or VIA transition metal in particular Zr, Ti, Hf, R and R¹ are
35 independently hydrocarbyl having 1-20 carbon atoms, halogen or other suitable

monovalent ligand; $m = 1-3$, $x = 0-3$ and $y = 0-3$ wherein the sum of m , x and y equal the oxidation state of M .

Preferred metallocenes are those wherein M is Zr, Hf or Ti, R_1R^1 are alkyl or halogen and $m = 2$.

5 Preferred metallocene complexes are those described in EP 129368, EP 206794 and EP 586167.

Particularly suitable are complexes in which the cyclopentadienyl nucleus is substituted by alkyl groups for example butyl groups.

10 A particularly suitable complex is bis(2-butyl) cyclopentadienyl zirconium dichloride.

The Ziegler component of the multisite catalyst may typically be a traditional Ziegler polymerisation catalyst well known to those skilled in the art. Preferably the Ziegler component of the multisite catalyst is one comprising atoms of titanium and halogen usually chloride and also preferably magnesium. Such 15 catalysts and their preparation will be well known to those skilled in the art.

The multisite catalyst is preferably supported and is most preferably supported on an inorganic support for example silica, alumina or magnesium chloride. The preferred support is silica.

20 The multisite catalyst may be supported by any traditional method of support. For example the support may preferably be initially impregnated by the Ziegler component prior to impregnation with the metallocene.

Preferably the silica support has been precalcined by heating before 25 impregnation.

The multisite catalyst may also comprise an activator. The preferred activator is aluminoxane, most preferably methyl aluminoxane (MAO). The activator is preferably present in an amount such that the ratio of metallocene to metal (aluminium) is in the range 1-10,000 : 10,000 : 1 but is preferably in the range 1-100 : 100:1.

30 The novel polyethylenes of the present invention are most suitably prepared by polymerisation of ethylene in the slurry phase in a batch mode of operation. The polymerisation is carried out in a single reactor using an inert solvent for example isobutane at a temperature in the range 80 - 110°C and at a pressure in the range 400 - 650 psig. The polymerisation preferably takes place in the presence of a cocatalyst for example an organoaluminium compound. The preferred cocatalyst is 35 a trialkylaluminium for example trimethylaluminium.

It has also been found possible to prepare the novel polyethylenes of the present invention by forming a blend of materials for example a blend of a metallocene derived polyethylene together with a low molecular weight component. The first component of the blend may be a polyethylene having a 5 molecular weight >200,000 and the second component may be a polyethylene having a molecular weight <200,000. The second component typically is a high density polyethylene. The metallocene derived polyethylene may be prepared using a metallocene complex having the general formula described above. In this respect however it has been found that hafnium metallocenes are most suitable for example 10 bis (2-propenyl) cyclopentadienyl hafnium dichloride.

The low molecular weight component typically has a molecular weight in the range 60,000-95,000.

In order to be processable in extrusion blow moulding pipe and film applications the primary requirements are that the polymer melt should be 15 extrudable and also that it should be resistant to instability or rupture.

The novel polyethylenes of the present invention exhibit these properties of extreme toughness and improved processability. This combination of properties therefore make the novel polymers suitable for use in a wide range of applications. In particular they may be used for high molecular weight blow moulding 20 applications such as large containers as well as pipe and tough film applications.

Thus according to another aspect of the present invention there is provided a pipe or film or moulded article comprising a polyethylene as hereinbefore described.

The novel polymer compositions were characterised by use of the following 25 experimental techniques.

Experimental Techniques

1. Toughness

Toughness was measured using a non-standard Charpy impact test and an impact test machine capable of measuring the load-deformation profile during the impact 30 event. The specimen was 55mm long, 6.7mm deep and 6mm thick and had a 1.7mm deep sharp notch machined centrally with respect to the length and leaving a ligament of 5mm behind the notch. Impact testing was performed using a span of 40mm and an impact speed of 1m/s over a range of temperature from 23C down to much lower temperatures. The lower test temperatures depend on the 35 toughness of the material; the higher the toughness, the lower the temperature

must be in order to achieve fracture of the specimen. Typically for the tougher materials, temperatures below -60C are required and down to as low as -120C. At least 5 data points were required in order to assess the toughness of the material and these must cover a temperature range of at least 20C.

5 For each test at a given temperature, the energy required to initiate crack growth was determined from the area under the load trace up to the point at which fracture occurs (denoted by a sudden load drop). This energy, $U_p(J)$, was then divided by $0.52*B*D$, where $B(mm)$ and $D(mm)$ are the specimen thickness and depth, respectively, to obtain the toughness $G_p(kJ/m^2)$. A graph was then drawn
10 of toughness in KJ/m^2 against temperature in degrees Celsius, from which a toughness value at -40C was derived. In most cases for tough materials, the data have been obtained at temperature below -40C and the toughness at -40C is derived by fitting a line of the form

$$G_p = A*(T+150)+5$$

15 to the data. The toughness at -40C, denoted $G_p(-40)$ is then given by

$$G_p(-40) = A*110+5$$

in the small number of cases where toughness can be measured at -40C, then the value quoted for $G_p(-40)$ is the measured value.

The value quoted is $G_p(-40)$ in units of kJ/m^2 .

20 2. **Dynamic Viscosity**

Samples for dynamic rheometry were prepared by compression moulding sheet (nominally 1-2mm thickness) using an electrically heated hydraulic press. The starting powder or pellet is placed between the pre-heated platens of the press (200C) and allowed to heat for 1 minute before being pressed for 2 minutes. The
25 heating is switched off, and the press water-cooled to ambient temperature before the moulding is released.

Dynamic frequency scans are carried out using a rotational rheometer (Rheometrics RDS2) equipped with 25mm diameter parallel plates enclosed in an environmental chamber. The environmental chamber is heated using nitrogen gas
30 to avoid excessive sample degradation during testing. A 25mm diameter disk is stamped from moulded sheet and placed between the pre-heated rheometer plates, which are then closed in such a way as to avoid the generation of excessive normal forces. The sample is trimmed and the oven closed to establish a testing temperature of 190C. A frequency scan is then performed at 10% applied strain
35 over the range 100 rad/s to 0.01 rad/s.

The dynamic viscosity (η') is then calculated at each testing frequency using standard equations [Draft International Standard ISO/DIS 6721/10].

Values of η' are quoted at frequencies of 100 rad/s ($\eta'(100)$, in units of Pa.s) and 0.01 rad/s ($\eta'(0.01)$ in units of kPa.s).

5 3. **Melt Mass-Flow Rate (MFR)**

Melt mass-flow rate of the materials is measured to ISO 1133:1997-condition 7.

The value quoted is MFR in dg/min.

4. **Die Swell**

10 Die swell is determined on solidified extrudate from a melt mass-flow rate test carried out according to ISO 1133:1997 - condition 7. Six cut-offs about 25mm in length, and free from air bubbles and distortion, are taken and allowed to cool evenly. The diameter of each cut-off is measured in two perpendicular directions, 6.35mm from the leading edge of the cut-off, using a dial gauge

15 micrometer. The die swell is calculated according to

$$\text{Die Swell} = 100 * (d - d_o) / d_o$$

where d is the mean diameter of the cut-off and d_o is the diameter of the die orifice in the melt flow rate apparatus. The average value of Die Swell for the six cut-offs is then calculated.

20 The value quoted is Die Swell in %.

5. **Annealed Density**

Annealed density for the materials is determined on extrudate from the melt flow rate evaluation in accordance with ISO1872/1-1986.

The value quoted is density in kg/m³.

25 6. **Weight Average Molecular Weight**

The distribution of molecular weights is first determined by size exclusion chromatography of the polymer dissolved in trichlorobenzene at 140C. A series of narrow polystyrene standards is used to calibrate the elution time, using the Polymer Handbook (3rd Edition) values for the Mark-Houwink parameters to

30 convert PS molecular weight to PE molecular weight. The weight average of the distribution is then calculated via the formula:

$$M_w = \Sigma w_i M_i / \Sigma w_i$$

w_i being the weight of the fraction of molecular weight M_i .

The value quoted is M_w .

35 The present invention will now be further illustrated by reference to the

accompanying examples.

Preparation of Catalyst

The following procedure was used to prepare a supported multisite (metallocene/Ziegler) catalyst.

5 A silica (ES70X) support (precalcined to 600°C for 6 hrs under N₂) was slurried in dry hexane at 55°C. A solution of dibutyl magnesium in heptane was added resulting in a 40g ES70X/350 ml hexane/28.4 mmol dibutylmagnesium slurry. After 1 hour 2.6 mmol butanol was added followed by 1.6 mmol TiCl₄. The solvent was subsequently removed under vacuum to give a dry catalyst

10 powder.

The resultant supported Ziegler catalyst was subsequently impregnated with a bis (n-butyl) cyclopentadienyl zirconium dichloride/MAO adduct (prepared by mixing both in toluene solution). The metallocene/MAO solution was added to the Ziegler catalyst followed by vacuum drying to give a dry catalyst powder.

15 The resultant supported multisite catalyst had the following analysis

Mg 1.12%

Ti 0.92%

Al 12.2%

Zr 0.38%.

20 The above catalyst was used to polymerise ethylene in a batch reactor in the presence of trimethylaluminium as cocatalyst. The polymerisation was performed in the slurry phase in isobutane. The following Examples 1-3 represent polymerisations under the conditions given in Table 1.

25 The polymer product was stabilised and compounded using a Prism lab scale twin screw extruder. Three passes through the compounder were used to ensure adequate homogeneity while avoiding molecular weight degradation.

TABLE 1

Example	1	2	3
Reactor pressure (psig)	600	600	600
Reactor temp. (°C)	85	85	85
Catalyst wt (g)	1.2	1.35	1.3
H ₂ pressure (psig)	10	4	2
Isobutane (litres)	40	40	40

Example 4

A high molecular weight polymer was prepared in accordance with the following procedure.

5 Silica, ES70X (preclaimed at 200°C under N₂ for 5 hrs) was impregnated with a slurry of MAO in toluene by refluxing at 115°C for 3 hours under N₂ followed by cooling to room temperature, filtering, washing and drying. The resultant support was then impregnated with bis (2-propenyl) cyclopentadienyl hafnium dichloride in dry toluene for 1 hr at ambient temperature followed again by filtration, washing with toluene and vacuum drying. The supported 10 metallocene/MAO catalyst had the following analysis:

Al 11.4%

Hf 0.66%.

A high molecular weight, high density polyethylene homopolymer was made using a blend of (a) the polymer prepared using the previously described 15 procedure and (b) a low molecular weight commercially available injection moulding grade polymer (weight average molecular weight of 75,000). The blend was prepared by dissolving the components in xylene at 125°C followed by stirring for 30 min. then precipitating the solution in acetone. The resulting product was dried and stabilised with 0.2% Ciba Geigy Irganox 1010.

20 The final blended product had the properties shown below in Table 2.

Example 5 (Comparative)

A high molecular weight, high density polyethylene homopolymer (Rigidex HM5420XP(H) sold by BP Chemicals) had the product properties listed in Table 2. The polymer was prepared using Phillips single site technology.

Example 6 (Comparative)

A high molecular weight, high density polyethylene homopolymer (Hizex 9200B sold by Mitsui Chemicals) had the product properties listed in Table 2. The polymer was prepared using typical Ziegler cascade technology.

30 The results clearly show the novel polymers of the present invention exhibit both extreme toughness and processability when compared with the prior art materials.

TABLE 2
POLYMER PROPERTIES

Example	Fracture Toughness (Gp) (kJ/m ²)	Dynamic Viscosity		MFR g/10 min (21.6 kg load)	Annealed Density (kg/m ³)	Weight Average M.Wt.	Die Swell %
		100 rad (Pa.s)	0.01 rad (kPa.s)				
1	27	1440	1080	1.49	961	501,000	22
2	40.3	2400	1340	0.55	952	548,000	21
3	51.2	2750	780	0.71	949	488,000	33
4	31.7	2300	520	0.66	948	375,000	28
5	19.2	1910	701	2.2	954	376,000	42
6	19.5	1980	699	1.3	955	392,000	21

Claims

1. A polyethylene having an annealed density in the range 900 to 980 Kg/m³ and a molecular weight greater than 200,000 characterised in that the polyethylene has
 - (a) an initiation fracture toughness (G_p) at -40°C of greater than 20 kJ/m²,
 - (b) a dynamic viscosity of <3000 Pa.s at 100 rad/sec (190°C) and < 3000 kPa.s at 0.01 rad/sec (190°C), and
 - (c) a mass flow rate (MFR) under 21.6 kg load (190°C) of 0.01 - 100g/10 min.
- 5 10 2. A polyethylene according to claim 1 having
 - (a) an initiation fracture toughness >25 kJ/m²,
 - (b) a dynamic viscosity <2500 Pa.s at 100 rad/sec and <1500 kPa.s at 0.1 rad/sec, and
 - (c) a MFR of 0.2 - 10 g/min
- 15 3. A polyethylene having an annealed density in the range 900-980 Kg/m³ and a molecular weight greater than 200,000 characterised in that the polyethylene has
 - (a) an initiation fracture toughness (G_p) at -40°C of greater than 20 kJ/m²
 - (b) a dynamic viscosity of <3000 Pa.s at 100 rad/sec (190°C) and <3000 kPa.s at 0.01 rad/sec (190°C), and
 - (c) a die swell in the range 10 - 80%.
- 20 4. A polyethylene according to claim 3 having a die swell in the range 20 - 40%.
- 25 5. A polyethylene according to any of the preceding claims having an

annealed density in the range 930 - 970 kg/m³ and a molecular weight >400,000.

6. A process for preparing a polyethylene according to any of the preceding claims comprising polymerising ethylene in the presence of a catalyst comprising a metallocene component and a Ziegler catalyst component.

5 7. A process according to claim 6 wherein the metallocene component has the general formula



wherein

10 Cp = substituted as unsubstituted cyclopentadienyl nucleus

M is a Group IVA, VA or VIA transition metal

R₁R¹ are independently hydrocarbyl, halogen or other suitable monovalent ligand,

m = 1-3

15 x,y = 0-3

and wherein the sum of m,x and y equal the oxidation state of M.

8. A process according to claim 7 wherein the metallocene is represented in the general formula by

20 M = Zr, Hf, Ti

R₁R¹ = alkyl or halogen, and

m = 2

9. A process according to claim 7 wherein the metallocene component is bis(n-butyl) cyclopentadienyl zirconium dichloride.

10. A process according to claim 6 wherein the catalyst comprises an activator.

25 11. A process according to claim 10 wherein the activator is an aluminoxane.

12. A process according to claim 6 wherein the catalyst is supported.

13. A process according to claim 12 wherein the support is silica.

14. A process according to claim 6 performed in the slurry phase in a batch mode of operation.

30 15. A process according to claim 6 performed in the presence of a cocatalyst.

16. A process according to claim 15 wherein the cocatalyst is an organoaluminium compound.

17. A polyethylene according to claim 1 comprising a blend of

(a) a polyethylene having a molecular weight >200,000 and

35 (b) a polyethylene having a molecular weight <200,000

18. A polyethylene according to claim 17 wherein the component (a) is prepared from a metallocene catalyst.
19. A polyethylene according to claim 18 wherein the metallocene is bis(2-propenyl) cyclopentadienyl hafnium dichloride.
- 5 20. A polyethylene according to claim 17 wherein the component (b) has a molecular weight in the range 60,000 - 95,000.
21. A film, pipe or molded article comprising a polyethylene as claimed in claims 1 or 3.

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INTERNATIONAL SEARCH REPORT

Inte .onal Application No
PCT/GB 99/00924

A. CLASSIFICATION OF SUBJECT MATTER
IPC 6 C08F10/02 C08F4/64 C08L23/06

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

IPC 6 C08L C08F

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practical, search terms used)

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X	WO 98 05422 A (MOBIL OIL CORP) 12 February 1998 see abstract see figure 1; examples 1,3 see page 9, line 4 - line 17 ---	1-3,6-16
X	EP 0 763 550 A (SHOWA DENKO KK) 19 March 1997 see page 27; examples 38,39; table 2 see page 28; examples 40,41; table 2 see page 16, line 22 - line 23 ---	1,2
X	WO 97 43323 A (DUN JOZEF J VAN ;MIYAMOTO AKIRA (JP); MATSUSHITA FUMIO (JP); CHUM) 20 November 1997 see page 115; examples 9,10; table 4 see page 109; examples 9,10 ---	1 -/-

Further documents are listed in the continuation of box C.

Patent family members are listed in annex.

² Special categories of cited documents :

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INTERNATIONAL SEARCH REPORT

Inte. onal Application No

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C.(Continuation) DOCUMENTS CONSIDERED TO BE RELEVANT

Category	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
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A	<p>WO 96 14358 A (DOW CHEMICAL CO) 17 May 1996</p> <p>see page 14, line 6 - line 13 see page 18, right-hand column; table I8 see page 13, line 18 - line 20 ---</p>	1-3,17, 21
A	<p>EP 0 783 022 A (MITSUI PETROCHEMICAL IND) 9 July 1997</p> <p>see page 11, line 45 - line 54 see page 16; table 1 see page 2, line 40 - line 43 -----</p>	3,4,17, 21

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